

A Closed Loop Process for the Endof-Life Electric Vehicle Li-ion Batteries

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Organization: Worcester Polytechnic Institute

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Project ID #: bat293

Overview

Timeline

- Project start date: Feb 2, 2016
- Project end date: Feb 15, 2018, NCE to May 15, 2018
- Percent complete: 100%

Budget

- Total project funding: \$1,024,740
 - DOE share: \$512,370
 - Contractor share: \$512,370
- Funding received in FY 2017: \$361,137
- Funding for FY 2018: \$169,510

Barriers

- Barriers addressed
 - Cost
 - Performance

Partners

- Interactions/ collaborations:

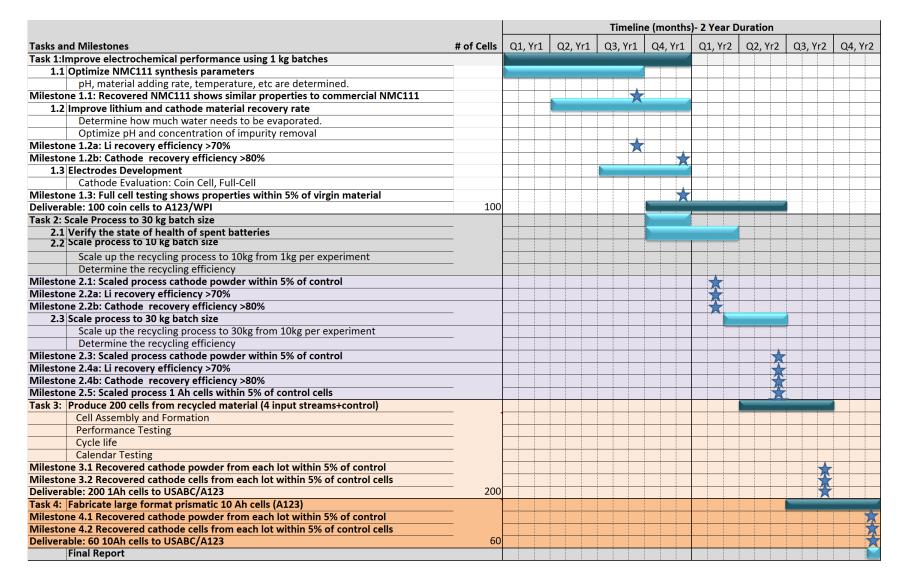
 A123 Systems, Battery

 Resourcers, Argonne National Laboratory, General Motors, Ford,
- FCA, SNT
- Project lead: WPI

Relevance and Project Objectives

- Recycle multiple 10 kg size batches of end of life EV batteries consisting of different incoming cathode chemistries
- Produce cells of a single chemistry that could be used in a PHEV battery, to be tested according to USABC's PHEV test methods
- Improve the performance of the recovered cathode materials so that they exhibit performance on level with current commercial materials
- Recycle other materials including steel, copper, aluminum, etc.

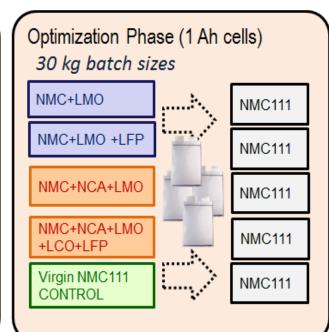
Milestones

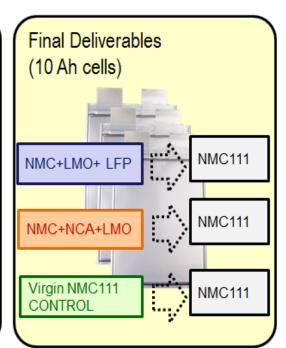


Cell Fabrication and Test Plan



- DCR impedance
- Rate capability
- Self discharge
- Cycle life trend
- Cath. Recov. Effic.
- · Li Recov. Effic.





Test Article	Total Made	Groups	USABC/ ANL	A123/ WPI	Comments
1 Ah NMC111/ gr cells	250	4	(4x10) 50 total	200	Less cells have been fabricated due to the low usage of materials.
10 Ah NMC111/ gr cells	60	3	(3x10) 30 total	30	Less cells have been fabricated due to the low usage of materials.

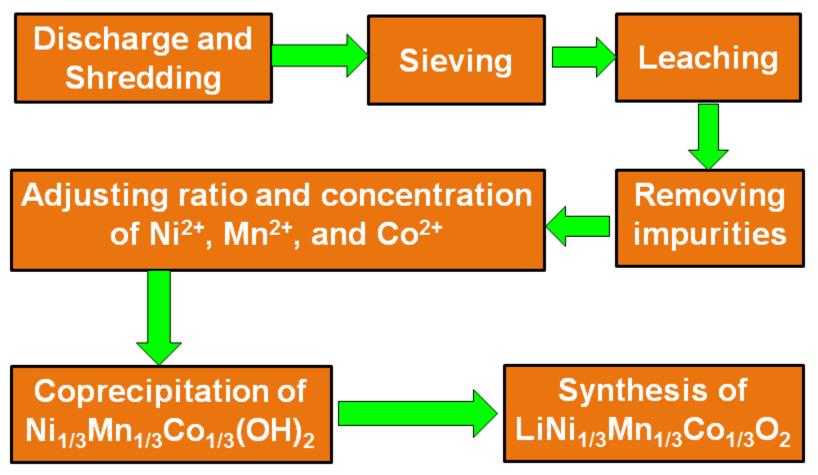
Approach: a Close Loop Process



Advantages:

- Any lithium Ion battery
- Any size and shape
- No sorting
- Synthesize new LiNi_xMn_yCo_zO₂ directly
- Ratio of Ni, Mn and Co can be specially tailored to customer demands

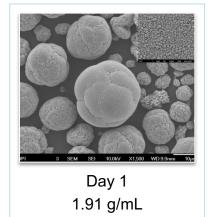
Technical Accomplishment and Progress: Recycling Process Has Been Developed

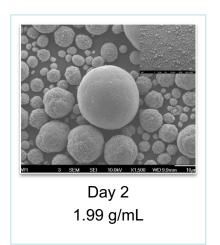


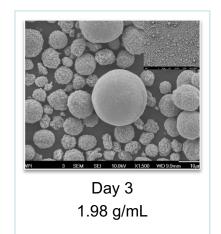
Recycling process is developed to offer a close loop process for the end of life EV batteries.

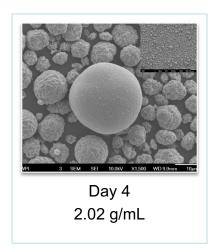
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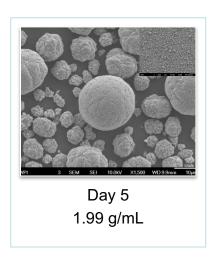
Morphology of Precursor (NMC Hydroxide)

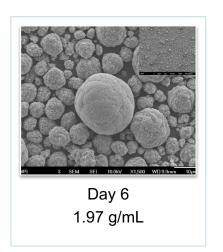


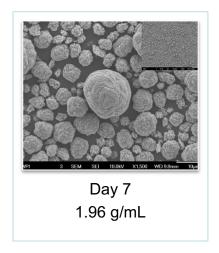






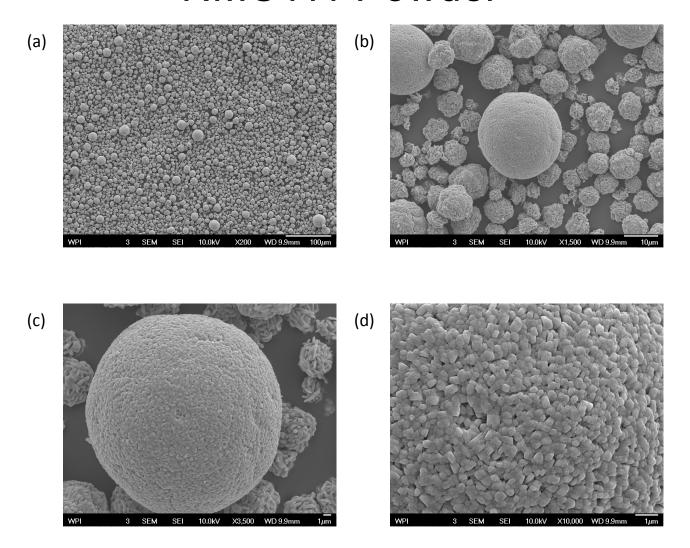






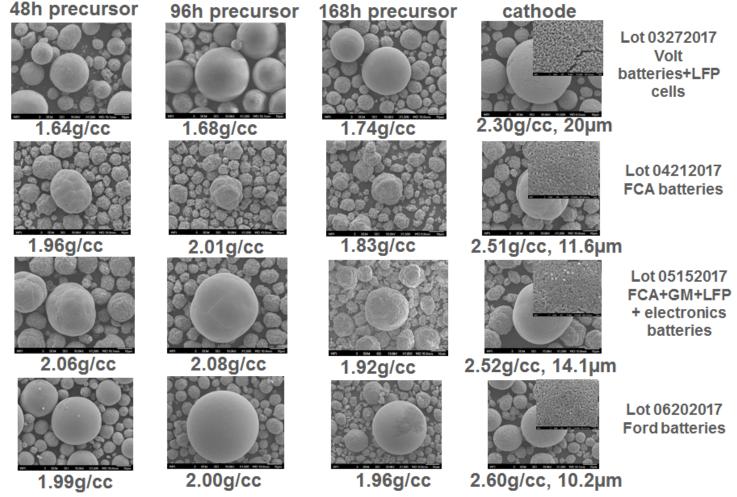
NMC precursor with good morphology has been synthesized with the recycled materials.

NMC111 Powder



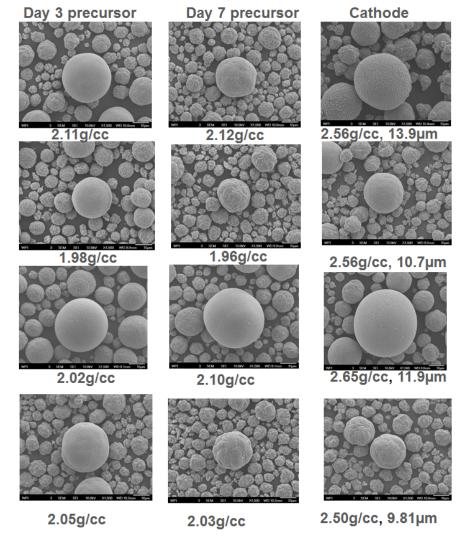
Spherical and high tap density (>2.5g/cc) NMC111 powder is synthesized from the recycling stream.

NMC111 from Different Recycling Streams (for 1Ah cells)



NMC111 powder has been synthesized from different recycling streams. The powder is used for 1Ah cells.

NMC111 from Different Recycling Streams (for 10Ah cells)



Lot 08112017
First
experiment
Ford Focus
batteries+LFP
cells

Lot 08302017 Second experiment Ford Fucus batteries+LFP cells

Lot 09192017 Third experiment FCA cells

Lot 10092017 Fourth experiment FCA cells NMC111
powder has
been
synthesized
from different
recycling
streams. The
powder is used
for 10Ah cells.

ICP Results-Impurity of NMC 111

Elements	Commercial NMC 111 Cathode (mol/L)	WPI NMC 111 Precursor (mol/L)	WPI NMC 111 Cathode (mol/L)
Ni	0.386	0.195	0.522
Mn	0.335	0.199	0.514
Co	0.365	0.199	0.515
Li	1.078	0.000	1.591
Na	0.014	0.000	0.000
Cu	0.000	0.000	0.000
Fe	0.000	0.000	0.000
Al	0.008	0.010	0.009
Mg	0.000	0.000	0.000

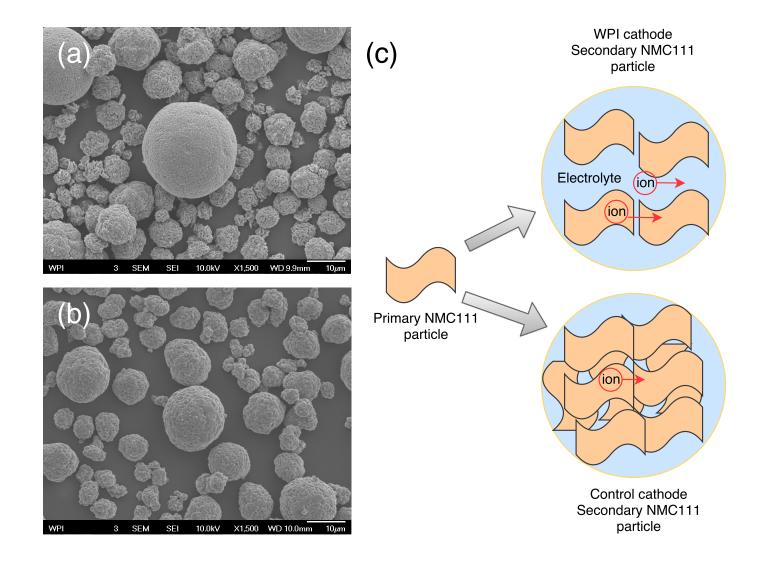
Recovered NMC111 precursor and powder have low impurity levels.

A123 Test Results (Coin Cells)

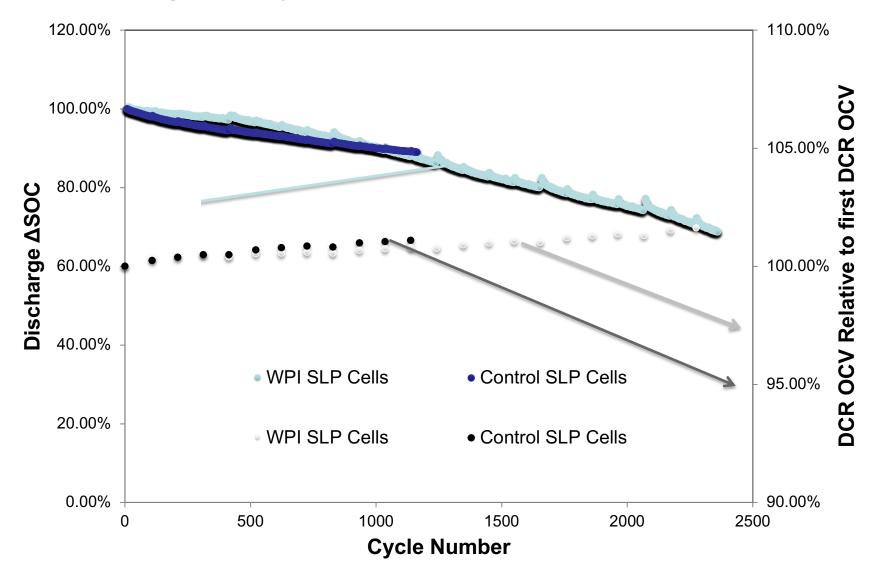
Test	Metric	Control Powd er (B)	09112017 8 kg	10182017 8 kg
Tap Density	g/cc	2.84	2.45	2.52
D50 PSD	um	9.2	11.7	11.2
BET	m2/g	0.28	0.40	0.43
FCC/ FDC	mAh/g	174.7/ 157.2	168.9/ 148.6	179.6/ 156.1
Efficiency	%	90.0	88.0	86.9
1C	mAh/g	130.9	136.3	139.2
2C	mAh/g	119.4	130.0	131.6
5C	mAh/g	40.4	107.5	111.2
Full coating		Complete	Complete	Complete

Recovered NMC111 powder has comparable performance comparing to the commercial powder. The high rate performance of recovered powder is better.

Possible Reason of Rate Capability Difference



Single Layer Pouch Cell Performance



Cost Analysis

10 tons/ day recycled

Cathode Production				
	Pyro	Hydro*(BR)	Virgin	
Cost	\$41.63	\$31.40	\$39.09	
Energy use in MJ per				
kg cathode material				
produced				
Total Energy	175.151	143.765	179.518	
Fossil fuels	162.011	134.362	165.545	
Coal	39.883	29.720	40.745	
Natural gas	83.952	70.093	83.408	
Petroleum	38.176	34.549	41.392	

5 tons/ day recycled

Cathode Production				
	Pyro	Hydro*(BR)	Virgin	
Cost	\$39.50	\$33.71	\$39.09	
Energy use in MJ per kg cathode material produced				
Total Energy	170.027	147.783	179.518	
Fossil fuels	157.115	138.380	165.545	
Coal	39.116	29.720	40.745	
Natural gas	80.478	70.093	83.408	
Petroleum	37.520	34.549	41.392	

- Modelling BRs
 economic process with
 ReCell from ARL
 -BRs process modelled
 with the hydro model
 -Pyro is the cost to
 make cathode
 materials via smelting
 EV batteries
- Input was 50% LMO
 50% NMC EV batteries
- Output was NMC111

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Responses to Previous Year Reviewers' Comments

<u>Comment 1:</u> The reviewer replied that this is a very practical project and approach to recycling but asked how is this recycling process different/novel/more cost-effective than Umicore's approach. The reviewer also stated that much more electrochemical testing is required to conclude that the recycled materials are of adequate quality.

<u>Response:</u> Umicore is using a pyrometallurgical process to recycle lithium ion batteries. In their process, they burn all the batteries and only recover Co, Ni and Cu. In our recycling process, we directly synthesize high quality NMC cathode powder (cathode powder accounts for >50% of the material value in lithium ion batteries.). In addition, our recycling process allows us to recover most of the materials (>90wt%).

<u>Comment 2:</u> The reviewer had two comments: First, the activities listed as remaining challenges are too sparse, elaborating that here is not enough electrochemistry data to jump to 2 Ah cells. The reviewer said that much more testing will be needed and that this should be done before scaling up the process. Second, a full economic model should be included to answer questions such as what do the waste streams look like now and is the cost of managing those included here.

<u>Response:</u> We only listed part of the electrochemistry data due to the limited slide number. We have done detailed economical model to show the economical feasibility of our recycling process.

<u>Comment 3:</u> The reviewer stated that there is good analytical comparison, but a lack of electrochemical evaluation and asked if the team has done a cost assessment.

<u>Response:</u> Our collaborator (A123 Systems) has done very detailed electrochemical testing with coin cells, single layer pouch cells, 1Ah cells and 10Ah cells.

Collaboration and Partners



Scale-up and commercialization



Fabricate commercial cells



Disassemble EV battery packs



Evaluate cells fabricated with recycled materials







Provide battery packs

Remaining Challenges and Barriers

Further Scale up to commercialization level

Proposed Future Work

- Recover other NMC materials with recycled streams
- Determine the impacts of different anode and adhesive materials
- Optimize the economical model

Summary

- The recycling technology offers a close loop process and can recycle Li-ion batteries with any shape, size and chemistry and sorting is not needed.
- The synthesized LiNi_{1/3}Mn_{1/3}Co_{1/3}O₂ from different recycling streams shows promising material and electrochemical properties.
- The process has been scaled up to 30kg spent batteries per experiment.
- Cost model shows the economical feasibility of the WPI recycling technology.